

Original article

# Impact of four different CO<sub>2</sub> injection schemes on extent of reservoir pressure and saturation

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**Abstract:**

This study investigates how four different injection schemes, (i. constant rate, ii. stepwise increasing rate, iii. stepwise decreasing rate, and iv. cyclic rate), constrained by the cumulative amount of CO<sub>2</sub> injected, affect the likely extent of pressure buildup and CO<sub>2</sub> plume, which play a role in the appraisal of environmental risk performance at CO<sub>2</sub> storage sites. This objective is achieved using a representative model of a realistic site consisting of multi-layer sandstone that is extremely permeable (between 1 to 2 Darcy) and separated by thin layers of shale extending laterally with sporadic discontinuities in form of perforations.

Results show that cyclic injection tends to keep the pore pressure lower than the other three injection schemes, while the highest pressure increase over the entire injection period (50 years) is observed with stepwise decreasing rate. The compressibility of CO<sub>2</sub> plays a role in attenuating the impact of fluctuating cyclic injection signals on pressure after 30 years of injection, where this time decreases by 5 years in case of heterogeneous scenario. Except for the cyclic injection scheme, all other three injection schemes lead to almost the same magnitude and areal extent of CO<sub>2</sub> saturation, while it shows a cyclic behavior in the case of the cyclic injection. Major observations are similar in both homogeneous and heterogeneous scenarios, although layered heterogeneity in the representative site introduces small differences in results.

The results imply that it would be preferable to store CO<sub>2</sub> using a cyclic injection scheme in storage reservoirs that may be prone to high pressure buildup during injection because of their geology (e.g., fractured shale reservoirs). These results also carry important implications for enhanced oil recovery (EOR) using CO<sub>2</sub> where the primary goal is to drive the oil out by increasing pore pressure; for EOR by CO<sub>2</sub>, stepwise decreasing rate would be most preferable as it leads to highest increase in pore pressure.

## 1. Introduction

The increasing production of carbon dioxide (CO<sub>2</sub>) at industrial scale either from energy (from fossil fuels, bio-renewable sources, etc.) or other industrial sources will required to be decarbonized under carbon-neutral economies by injecting into geologic formations for either enhanced oil recovery or pure sequestration. Appraisal of environmental risk performance for geologic CO<sub>2</sub> storage (GCS) requires assessing the impact of the pore pressure increase and CO<sub>2</sub> saturation as a potential risk. Specifically, assessing this risk is required to ensure that the geologic storage systems perform in conformance with expectations and engineering tolerances. In this regard, many studies have investigated the behavior of these systems (Heath and McPherson, 2004; Shipton et al., 2004; Kim, 2008; Bachu and Celia, 2009; Nordbotten et al., 2009; Xiao et al., 2009; Carey et al., 2010; Bateman

et al., 2011; Celia and Nordbotten, 2011; Ellis et al., 2011; Bhowmik, 2012; Birkholzer et al., 2014, 2015; Singh and Srinivasan, 2014a, 2014b; Singh, 2014, 2017; Huerta et al., 2015; Oldenburg et al., 2016; Wolterbeek et al., 2016; Singh and Huerta, 2017; Singh and Islam, 2018). However, there is no study known to the author's knowledge that investigates the extent of pressure buildup and CO<sub>2</sub> plume saturation for different injection schemes that is constrained by the total amount of CO<sub>2</sub> injected. Out of the four injection schemes investigated here, only cyclic injection scheme, also known as huff-n-puff, has been investigated from the perspective of oil recovery in terms of the shut-in time (soaking time), injection rates, number of wells, etc (Song and Yang, 2013; Yu et al., 2016; Zuloaga et al., 2017; Fragozo et al., 2018).

This study investigates the spatio-temporal extent of pressure buildup and CO<sub>2</sub> saturation plume as a function of



four different injection schemes (i. constant rate, ii. stepwise increasing rate, iii. stepwise decreasing rate, and iv. cyclic rate) to understand how the variation in injection rate, by constraining the cumulative amount stored, affects the reservoir risk. The numerical metrics used to study the spatio-temporal extent of pressure buildup and CO<sub>2</sub> saturation plume are discussed under next section. In the results section, the spatio-temporal extent of pressure buildup and CO<sub>2</sub> saturation plume are obtained for four injection schemes, considering both homogeneous and heterogeneous geology of the site, and their implications on pure CO<sub>2</sub> storage and/or EOR are discussed. Finally, the study is summarized and conclusions are presented.

## 2. Method and approach

Generally, it is not possible to study the behavior of the pressure buildup and CO<sub>2</sub> plume evolution in most real reservoirs using analytical or semi-analytical solutions (Mathias et al., 2011; Bandilla et al., 2012; Mukhopadhyay et al., 2012; Mohamed, 2013; Yang et al., 2013) that assume the reservoir is homogeneous, ideal in geological structure, and of infinite size. These assumptions render their use for real reservoirs invalid, which are heterogeneous, non-ideal in geological structure, and are of finite size. Therefore, to study pressure buildup and CO<sub>2</sub> plume evolution in a realistic reservoir, we use the following two metrics (Bromhal et al., 2014) that are formulated mathematically here.

### 2.1 Spatio-temporal extent of pressure buildup and saturation

Two metrics that define the spatio-temporal extent of pressure buildup and CO<sub>2</sub> saturation plume, considered as important indicators of storage/risk relationships (Bromhal et al., 2014), were used in this study: i) the area of pressure buildup in the storage reservoir over time, and ii) the area of CO<sub>2</sub> saturation over time. Each is described in detail below.

#### 2.1.1 Spatio-temporal extent of pressure buildup

Buildup in pressure can potentially drive CO<sub>2</sub> and/or brine out of a storage reservoir, which could impact ground water aquifers and other subsurface resources. Pressure buildup could also potentially cause increase in effective stress inside the storage site that can lead to seismic events. The evolution of the area of pressure buildup is a metric that suggests how a site's storage risks evolve over time.

For each scenario,  $\Delta P$  was determined relative to the initial reservoir pressure prior to initiation of CO<sub>2</sub> injection. The spatio-temporal extent of pressure buildup is determined relative to four thresholds (Bromhal et al., 2014) for each site: 0.01 MPa, 0.1 MPa (a small but measurable pressure increase), 0.5 MPa, and 1.0 MPa (a threshold approximately sufficient to drive fluids from a storage reservoir to an above-zone aquifer for many scenarios). Even though these thresholds are useful as rule-of-thumb thresholds, real values will be site and case specific.

The behavior of this metric is explored by calculating an effective area of the pressure buildup ( $A_{\Delta P}$ ), where  $A_{\Delta P}$  is the projection onto the XY plane of the portion of the reservoir with a  $\Delta P$  above a given threshold. First, spatial coordinates of the region inside a model are calculated where the differential pressure buildup is greater than a threshold pressure. A specific pressure buildup is the difference of pressure between its current state ( $P[x, y, z, t]$ ) and the initial state ( $P[x, y, z, 0]$ ):

$$\Delta P[x, y, z, t] = P[x, y, z, t] - P[x, y, z, 0] \quad (1)$$

If region inside this domain where differential pressure buildup is greater than a specific threshold is represented as  $C_P$ , we can write:

$$C_P[x, y, z, t] = \begin{cases} 1 & \text{when } \Delta P[x, y, z, t] \geq \Delta P_{\text{threshold}} \\ 0 & \text{otherwise} \end{cases} \quad (2)$$

Now, the effective area of the pressure buildup is calculated by projecting this region represented by  $C_P$  on the XY plane and integrating it along the X and Y directions. Then, the projection of  $C_P[x, y, z, t]$  to the XY plane,  $proj_{C_P}[x, y, t]$ , is given as follows:

$$proj_{C_P}[x, y, t] = \begin{cases} 1 & \text{when } C_P[x, y, z, t] > 0 \text{ for any } z \\ 0 & \text{when } C_P[x, y, z, t] = 0 \text{ for all } z \end{cases} \quad (3)$$

And the area of the pressure buildup, which will depend on the value of the pressure threshold, can be calculated as:

$$A_{\Delta P}[t] = \int_{x=-\infty}^{\infty} \int_{y=-\infty}^{\infty} proj_{C_P}[x, y, t] dy dx \quad (4)$$

For this work, this integral was estimated through a summation involving the discrete grid of a numerical reservoir model and using an early version of the REV tool (King, 2016) developed by the National Risk Assessment Partnership (NRAP).

#### 2.1.2 Spatio-temporal extent of CO<sub>2</sub> saturation

Mobile free-phase CO<sub>2</sub> (above residual saturation) carries a potential risk of migrating outside of primary storage reservoir because of buoyant driving force. The evolution of the area of CO<sub>2</sub> saturation plume is another metric that suggests how a site's storage risks evolve over time, especially given the uncertainty in the critical threshold for mobility of free-phase CO<sub>2</sub>.

The spatio-temporal extent of the CO<sub>2</sub> plume is considered relative to specific saturation thresholds, which in this work is determined relative to four CO<sub>2</sub> saturation thresholds for each site: 0.1 (irreducible CO<sub>2</sub> saturation that must be exceeded in a reservoir before the CO<sub>2</sub> phase becomes mobile), 0.3, 0.5, and 0.7 (maximum CO<sub>2</sub> saturation that can be present with residual water). The effective area of the CO<sub>2</sub> plume ( $A_s$ ) was derived by projecting onto the XY plane the CO<sub>2</sub> plume with saturation above a certain threshold value,  $S_{\text{threshold}}$ . If  $S_{CO_2}$  is the saturation plume and the region where differential

saturation is greater than a specific threshold is represented as  $C_s$ , then we can write:

$$C_s[x, y, z, t] = \begin{cases} 1 & \text{when } S_{CO_2}[x, y, z, t] \geq S_{\text{threshold}} \\ 0 & \text{otherwise} \end{cases} \quad (5)$$

Now, the effective area of the saturation plume is calculated by projecting this region represented by  $C_s$  on the XY plane and integrating it along the X and Y directions. The projection of  $C_s[x, y, z, t]$  to the XY plane,  $proj_{C_s}[x, y, t]$ , is given as following:

$$proj_{C_s}[x, y, t] = \begin{cases} 1 & \text{when } C_s[x, y, z, t] > 0 \text{ for any } z \\ 0 & \text{when } C_s[x, y, z, t] = 0 \text{ for all } z \end{cases} \quad (6)$$

And the CO<sub>2</sub> plume area above a threshold can be calculated as:

$$A_s[t] = \int_{x=-\infty}^{\infty} \int_{y=-\infty}^{\infty} proj_{C_s}[x, y, t] dy dx \quad (7)$$

As with the area of saturation above, these values were numerically estimated using an early version of NRAP's REV tool.

## 2.2 Storage site

This study uses a representative model of a real site that is quite popular with the community studying CO<sub>2</sub> storage; a multi-layer sandstone with shale baffles as shown in Fig. 1. Although the geological structure used in this study is realistic, it is not the actual model of the site, therefore, we refer to this site shown in Fig. 1 as site-S. The site is deeper than 800 m, a minimum depth required for the CO<sub>2</sub> to exist in supercritical state (critical pressure 7.28 MPa and critical temperature 31.19 °C) because the hydrostatic pressure below 800 m is greater than the CO<sub>2</sub> critical pressure.

Examining the risk behavior of this site with four variations in injection rates, and constraining the cumulative amount stored, allows investigating how different injection schemes affect the likely extent of pressure buildup and CO<sub>2</sub> plume that impact the reservoir risk.

The dimensions of site-S are 640 m × 1.18 km along the xy-plane and its depth varies between 803 m and 1341 m, and having an uneven top surface with multiple structural highs. The geology of site-S constitutes a late-Miocene/early-Pliocene formation, overlain by clay-rich sediments and underlain by shaly sediments, which is represented by 51 simulation layers. Site-S is extremely permeable (permeability varying between 1 to 2 D) and the permeable layers are separated by thin layers of shale corresponding to mudstones. The thickness of the thin shale layers is typically 1 to 1.5 m and they extend laterally along the reservoir with baffles in the form of perforations. The permeability along the y-direction is similar to the permeability along the x-direction, whereas the permeability along z-direction is one-tenth of the values along the x-direction. The porosity in site-S is assumed to be uniform (20%) throughout the volume of the reservoir.

The heterogeneity of the site is characterized using Dykstra-Parsons coefficient (Dykstra and Parsons, 1950), which is the most common measure used to characterize heterogeneity in the oil and gas industry (Jensen and Currie, 1990). Dykstra-Parsons coefficient ( $V_{dp}$ ) is sometimes also referred to as coefficient of permeability variation and the definition of  $V_{dp}$  is given as follows:

$$V_{dp} = \frac{\ln(k)_{0.50} - \ln(k)_{0.16}}{\ln(k)_{0.50}} \quad (8)$$

Where,  $k_{0.50}$  and  $k_{0.16}$  are the median permeability value and permeability value at one standard deviation below median permeability, respectively. The minimum and maximum value of  $V_{dp}$  is 0 and 1, respectively, which represent homogeneous medium and "infinitely" (hypothetically) heterogeneous medium, respectively. Assuming that heterogeneous permeability ( $k$ ) is log-normally distributed with mean  $\mu$  and standard deviation  $\sigma$ , the above formulation of  $V_{dp}$  can be re-written as following:

$$V_{dp} = 1 - \exp(-\sigma), \text{ where } \ln(k) \sim N(\mu, \sigma^2) \quad (9)$$

The robustness of  $V_{dp}$  as a heterogeneity measure lies in its assumption that the permeability data is log-normally distributed, which is actually true as many reservoirs have nearly log-normal permeability distributions (Jensen and Currie, 1990). The  $V_{dp}$  of permeability heterogeneity for site-S is 0.92.

### 2.2.1 Initial reservoir conditions and flow parameters

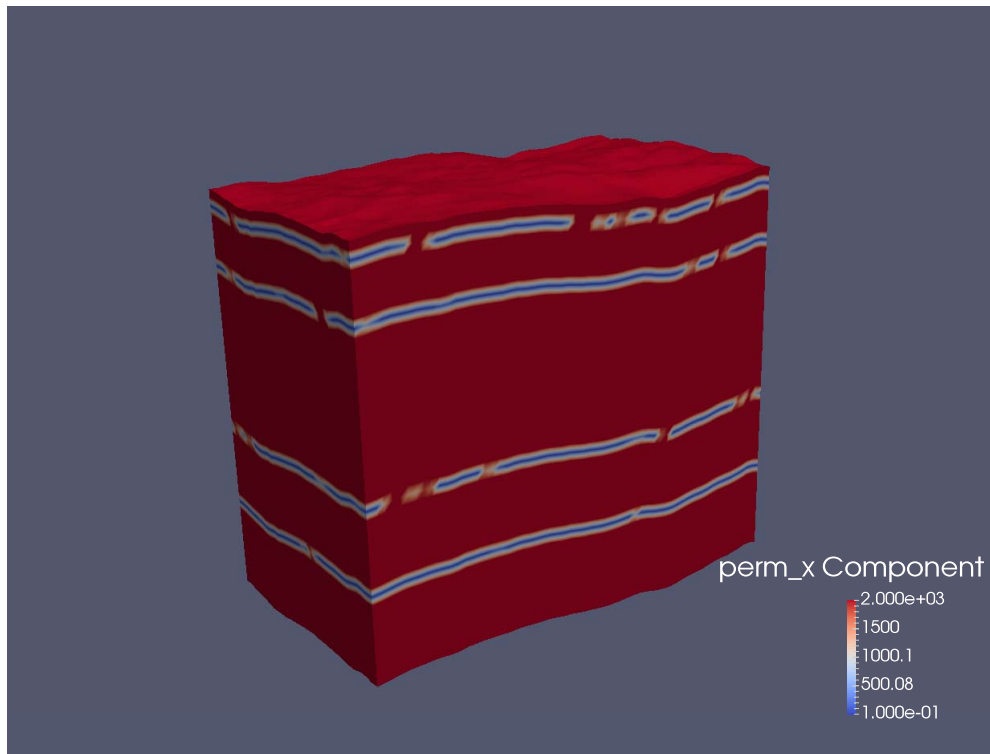
All the four injection schemes (constant rate, stepwise increasing rate, stepwise decreasing rate, and cyclic rate) assumed CO<sub>2</sub> injection over a period of 50 years followed by 250 years of post-injection observation period. Prior to initiation of CO<sub>2</sub> injection, hydrostatic equilibrium was established in the reservoir by enforcing zero mass flux at all side boundaries, and a gentle geothermal gradient (25 °C/km) was imposed along the vertical direction. The four variable injection schemes are shown in Fig. 2, where the total CO<sub>2</sub> injection over a period of 50 years for all the four injection schemes was 5 million tonnes.

The operating and initial reservoir conditions for this site are shown by Table 1.

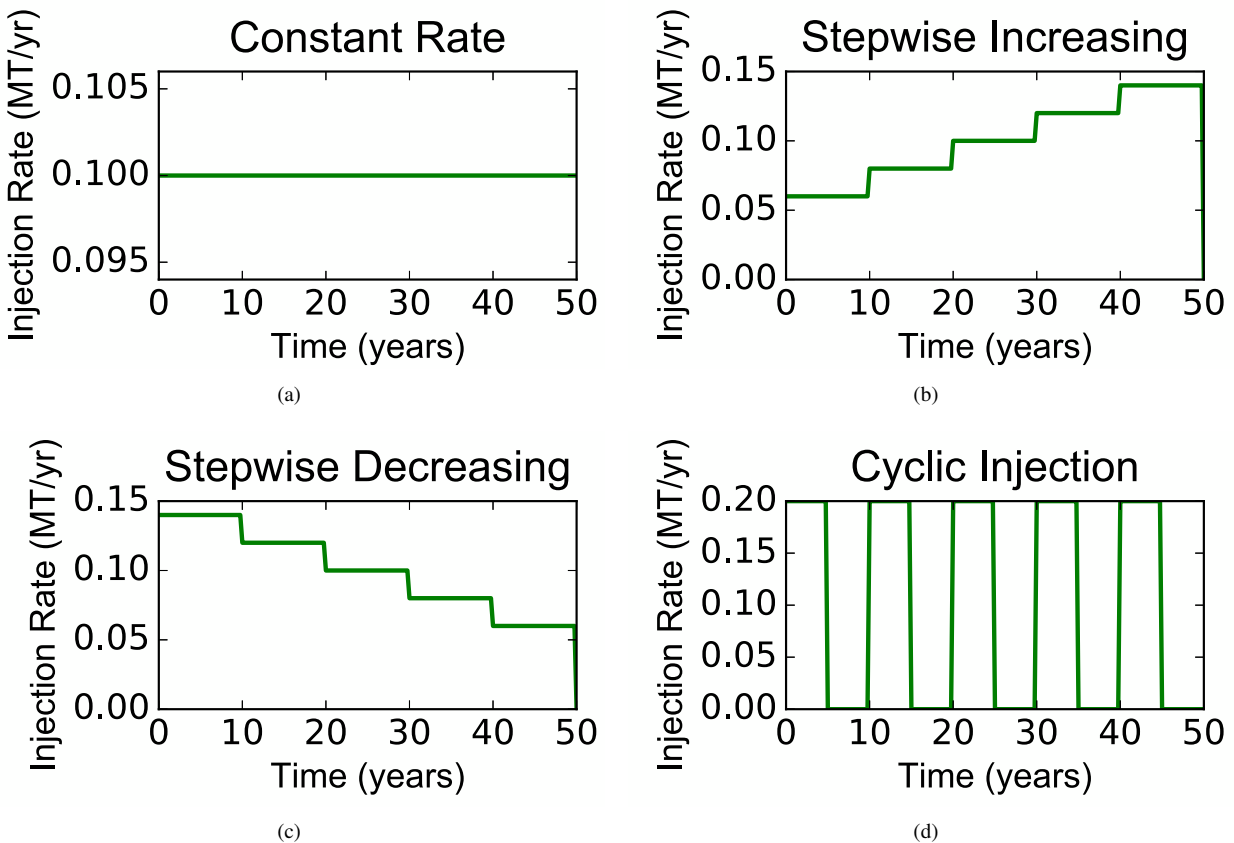
We used experimental relative permeability of liquid CO<sub>2</sub> and water from Dempsey et al. (2014) who compiled experimental datasets from several sources (Bachu and Bennion, 2007; Perrin and Benson, 2009; Krevor et al., 2012; Berg et al., 2013) and used a best-fit curve (minimum mean squared error) through those datasets, as shown in Fig. 3. This best-fitted experimental relative permeability curve has an irreducible saturation of 0.3 and 0.1 for water and CO<sub>2</sub>, respectively, endpoint relative permeability values of 0.8 and 1.0 for CO<sub>2</sub> and water, respectively, and exponent of 3.1 for both curves (Fig. 3).

### 2.2.2 Boundary conditions

Past studies for CO<sub>2</sub> storage related studies (e.g.,



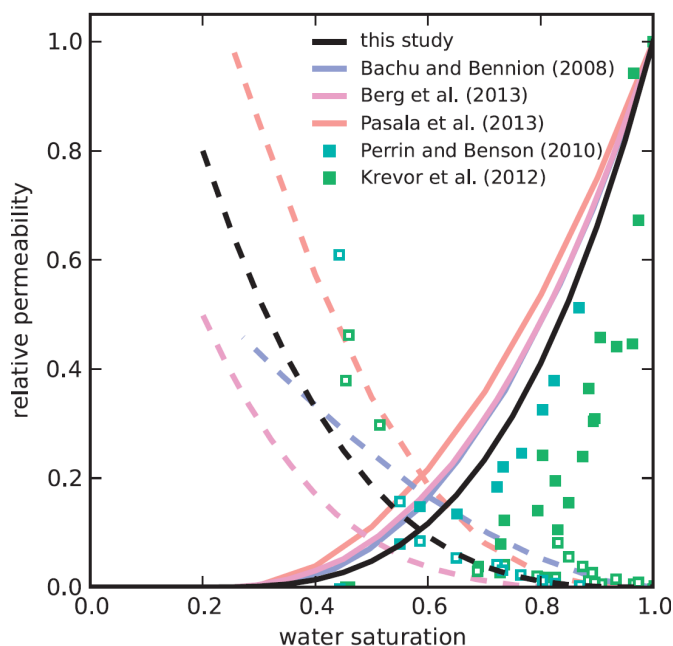
**Fig. 1.** Simulation model (exaggerated by a factor of 2 along  $z$ -axis) of Site-S depicting permeability (in mD) along  $x$ -direction (with arithmetic and geometric mean value of  $\sim 1,860$  and  $1,026$  mD). The blue layers are shale (extremely low permeability) with some baffles that may allow flow. Pore volume of both homogeneous and heterogeneous models are  $\sim 75 \times 10^6$  m<sup>3</sup>. The  $V_{dp}$  of permeability heterogeneity is 0.92. The assumed permeability of a homogeneous scenario is 200 mD.



**Fig. 2.** Four different injection schemes (constant rate, stepwise increasing, stepwise decreasing, and cyclic injection, respectively) used in this study. The cumulative amount of CO<sub>2</sub> injected in all these four injection schemes is equal to 5 million tonnes.

**Table 1.** Reservoir operating and initial conditions.

Properties of site-S		Values
Areal dimension (km <sup>2</sup> )	--	0.64 × 1.18
Depth (m)	--	803-1341
Pore volume (×10 <sup>6</sup> m <sup>3</sup> )	Homogeneous	75
	Heterogeneous	75
Initial pressure (MPa)	--	10
Initial temperature (°C)	--	40
Initial water saturation (%)	--	100
Constant injection rate (MT/yr)	--	0.1
Total injection (MT)	--	5
Heterogeneity	Arithmetic mean porosity	0.2
	Arithmetic mean permeability (mD)	1,860
	Geometric mean permeability (mD)	1,026



**Fig. 3.** Relative permeability curves (Dempsey et al., 2014) for supercritical CO<sub>2</sub> (dashed black curve) and water (solid black curve) used in this study. The experimentally-fitted relative permeability was used as a general representative of liquid CO<sub>2</sub> and water flow in this study.

Birkholzer and Zhou, 2009; Doughty, 2009; Zhou et al., 2009; Zhou and Birkholzer, 2011) have used Dirichlet (constant pressure/open flow) boundary conditions, including a benchmark study by Class et al. (2009) that assumes Dirichlet conditions equal to initial reservoir conditions for lateral boundaries and no-flow for the top and bottom boundaries. For this reason, this study assumes open-flow (Dirichlet) to brine and CO<sub>2</sub> across the four side boundaries and no-flow across the top and bottom boundaries to represent extensive and continuous shale sealing over and under each site.

The injector for site-S is located at the bottom layer of the reservoir and in the middle of the XY plane as a single node. Only one injector is placed in the middle to avoid the effects of pressure interference from multiple injectors

that may distort the natural pattern of pressure evolution, and complicate interpretation of simulation results (e.g., Birkholzer and Zhou, 2009; Zhou and Birkholzer, 2011).

### 2.3 Numerical modeling description and simulation scenarios

Reservoir simulations were performed for two-phase, immiscible and non-isothermal flow of CO<sub>2</sub> and brine at the continuum scale without considering any chemical reactions and CO<sub>2</sub> dissolution in brine as these effects are unlikely to affect (Singh, 2017) the global behavior of the CO<sub>2</sub> at reservoir scale mainly because these effects are local in nature and their rate of mass transfer is quite slow (Kumar et al., 2005). Also,



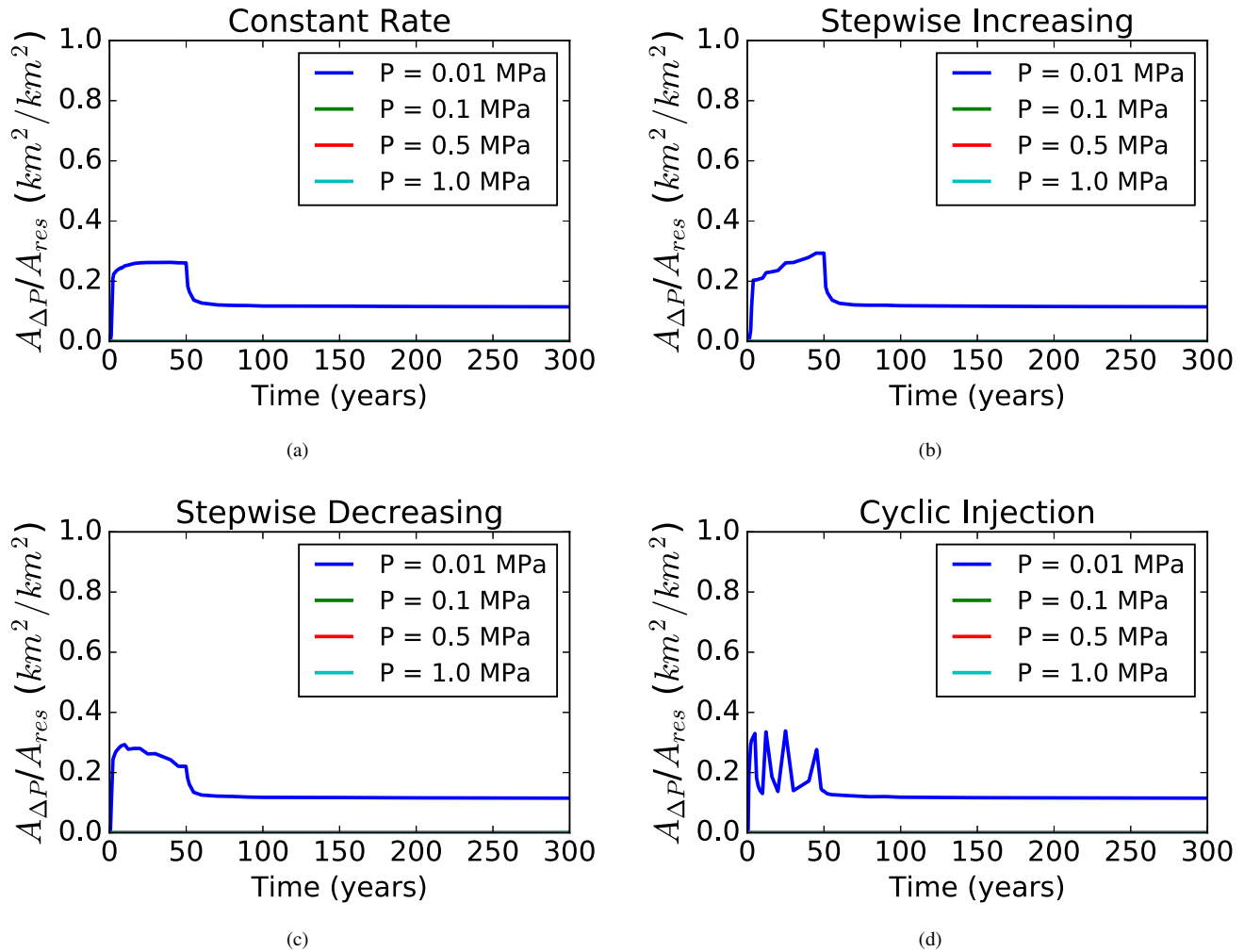


Fig. 4.  $A_{\Delta P}(t)/A_{res}$  with constant, stepwise increasing, stepwise decreasing, and cyclic injection rates.

it is assumed that capillary pressure between supercritical  $\text{CO}_2$  and brine is negligible, which is not an unrealistic assumption at field-scale with large pore sizes and the interfacial tension between  $\text{CO}_2$  and brine that decreases with pressure (e.g., Alkan et al., 2010).

A finite-element heat and mass (FEHM) transfer simulator developed by Los Alamos National Laboratory was used to study the two-phase supercritical  $\text{CO}_2$  and brine mixture in porous media. FEHM (Zyvoloski et al., 2011) solves heat and mass conservation equations for multi-phase, multi-fluid flow in porous media using an efficient, node-centered control volume implementation. Fluid properties of  $\text{CO}_2$  are dynamically calculated in FEHM using spatial and temporal variation in pressure and temperature. CPU computational time to complete each simulation run using a single processor ranged up to 96 hours.

The evolution of pressure pulse and saturation plume in site-S was investigated for four injection schemes (constant rate, stepwise increasing rate, stepwise decreasing rate, and cyclic rate) using geological models considering: i) homogeneous and isotropic scenario, and ii) heterogeneous scenario. For the homogeneous and isotropic scenario, permeability and

porosity were assumed to be 200 mD and 0.2, respectively, which results in similar pore volume ( $75 \times 10^6 \text{ m}^3$ ) as that of heterogeneous geology.

### 3. Results and discussions

Spatio-temporal extent of pressure buildup and  $\text{CO}_2$  saturation plume are computed for the site-S under two scenarios of homogeneous and heterogeneous geology, respectively. Results for these two metrics are obtained for the four injection schemes (constant rate, stepwise increasing rate, stepwise decreasing rate, and cyclic rate) while holding constant the total amount of  $\text{CO}_2$  injected. Dirichlet boundary condition (constant pressure/open flow) was used as it has been used by other studies (e.g., Birkholzer and Zhou, 2009; Class et al., 2009; Doughty, 2009; Zhou et al., 2009; Zhou and Birkholzer, 2011) that suggest it to be a realistic boundary condition for  $\text{CO}_2$  storage studies.

#### 3.1 With homogeneous model

Fig. 4 shows the areal extent of pressure buildup for

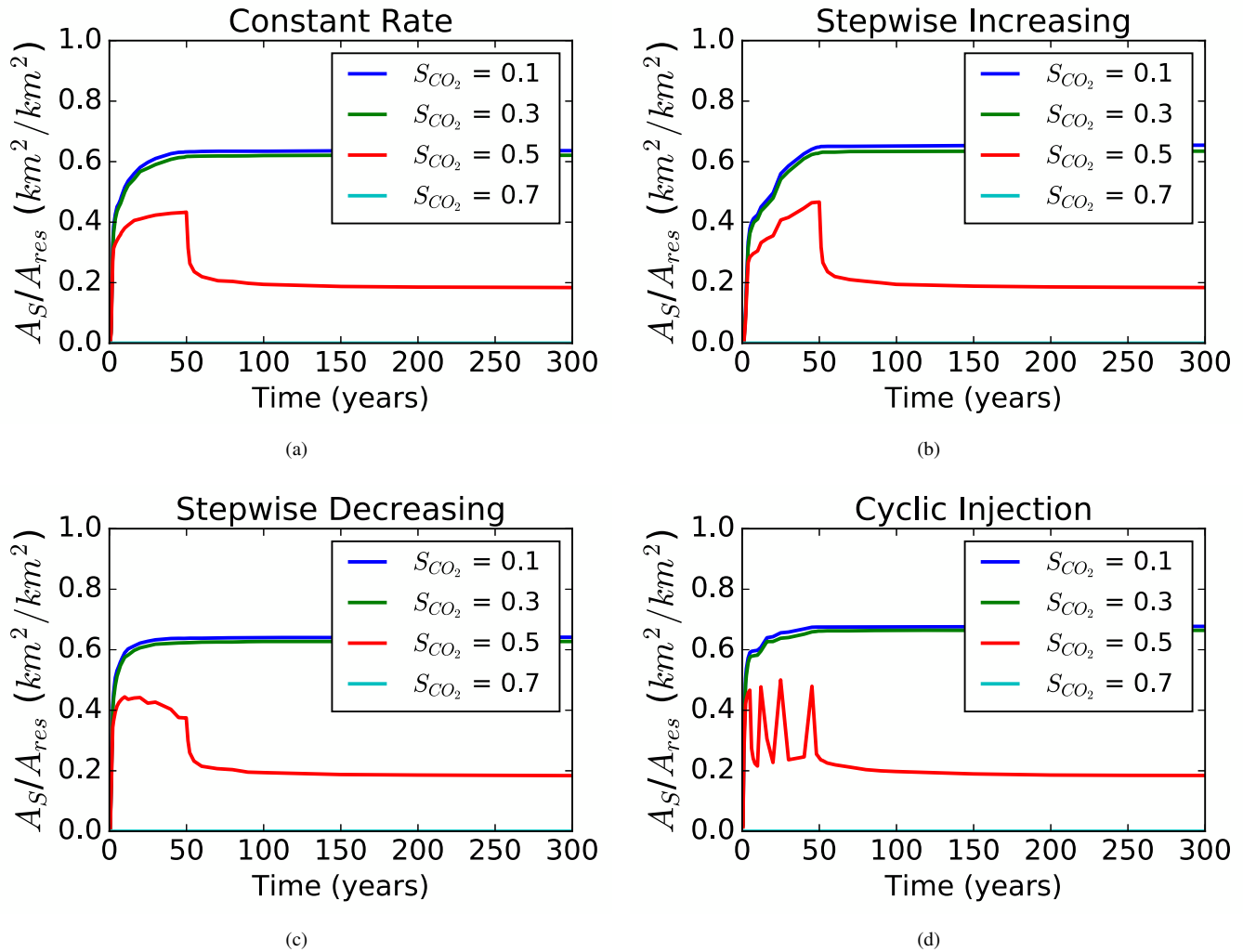


Fig. 5.  $A_S(t)/A_{res}$  with constant, stepwise increasing, stepwise decreasing, and cyclic injection rates.

the site with four different injection schemes considering geologically homogeneous case with four pressure thresholds ranging from 0.01 to 1 MPa. Fig. 5 shows the areal extent of CO<sub>2</sub> saturation plume with four different injection schemes considering geologically homogeneous case with four saturation thresholds ranging from 0.1 to 0.7. The variation of pore pressure (normalized as  $\frac{P-P_{min}}{P_{max}-P_{min}}$  to illustrate the variability due to < 1 MPa pressure buildup) with four injection schemes and comparison of normalized variation in both pressure and saturation are shown in section 3.1.2.

### 3.1.1 Spatio-temporal extent of pressure buildup and CO<sub>2</sub> plume

Except for the cyclic injections scheme, all other three injection schemes show a smooth variation in areal extent of pressure buildup and CO<sub>2</sub> saturation, while cyclic injection scheme introduces fluctuations in the areal extent of both pressure buildup and saturation. Although stepwise increasing and decreasing rates lead to subtle (very minute) wavering in the two variables plotted in Figs. 4 and 5, they are not significant. The extent of pressure buildup for  $P > 0.01$  MPa

was negligible, therefore, the three legends for  $P = 0.1, 0.5, 1.0$  MPa are not visible in Fig. 4.

### 3.1.2 Variability in pressure buildup and saturation

Fig. 6 shows that cyclic injection tends to keep the pore pressure lower than the other three injection schemes, while the highest pressure increase over the entire injection period (50 years) is observed with stepwise decreasing rate. This figure also shows that the fluctuations in the cyclic injection rate are not transmitted to pore pressure for the entire cycle of the injection period. This is because of the compressibility of CO<sub>2</sub> attenuates the impact of fluctuating injection rates that results in dampening the pressure.

Fig. 7 shows that the normalized CO<sub>2</sub> saturation follows the behavior of the pressure increase, i.e., the stepwise decreasing rate maintains the highest CO<sub>2</sub> saturation value over the entire injection period, and the cyclic fluctuations in the pressure (for cyclic injection rate) are also mimicked by the CO<sub>2</sub> saturation, although the fluctuations in the saturation are not as pronounced as the fluctuations in pressure (Fig. 7).

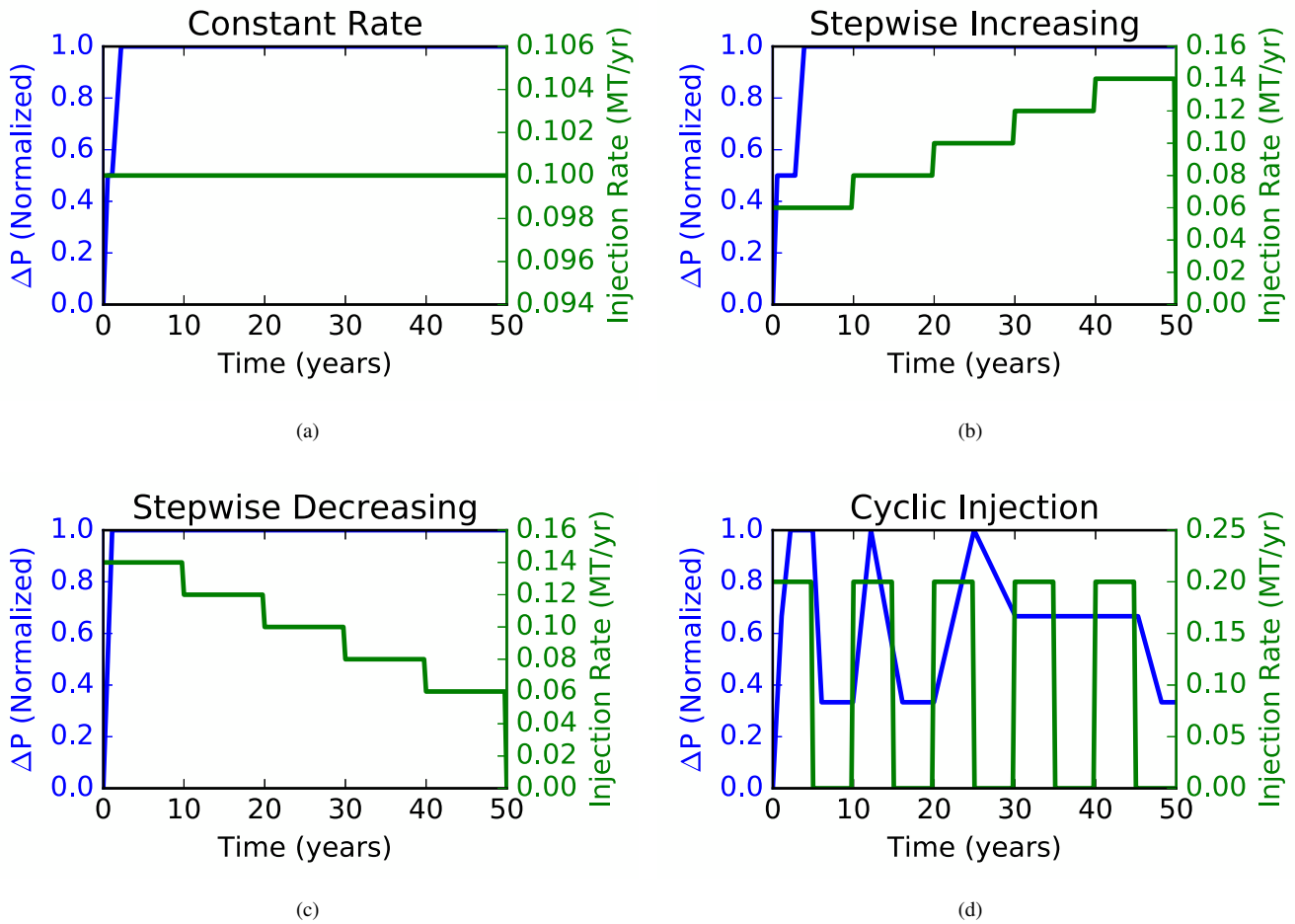
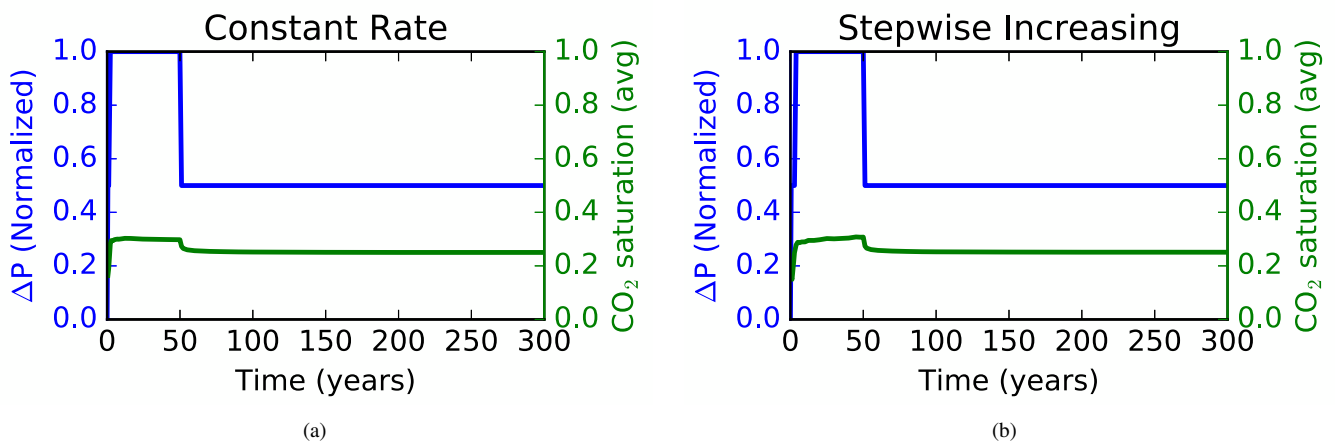


Fig. 6. Average pore pressure and injection rates with constant, stepwise increasing, stepwise decreasing, and cyclic injection rates.





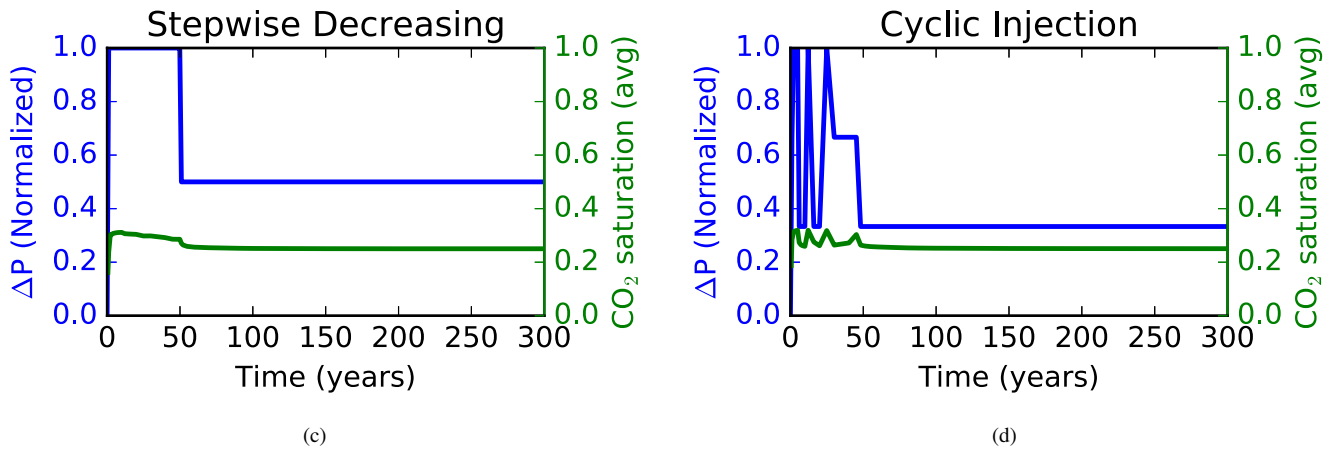


Fig. 7. Average pore pressure and average saturation with constant, stepwise increasing, stepwise decreasing, and cyclic injection rates.

### 3.2 With heterogeneous model

Fig. 8 shows the areal extent of pressure buildup for the site with four different injection schemes considering geologically homogeneous case with four pressure thresholds ranging from 0.01 to 1 MPa. Fig. 9 shows the areal extent of CO<sub>2</sub> saturation plume with four different injection schemes considering geologically homogeneous case with four saturation thresholds ranging from 0.1 to 0.7. The variation of pore pressure (normalized to illustrate the variability) with four injection schemes and comparison of variation in both pressure and saturation are shown in section 3.2.2.

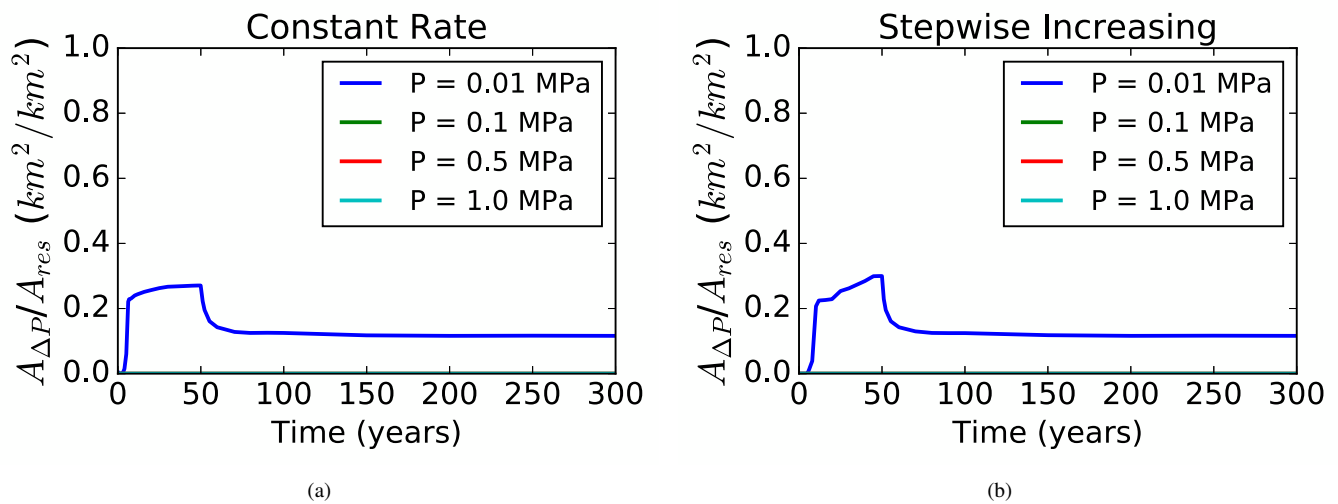
#### 3.2.1 Spatio-temporal extent of pressure buildup and CO<sub>2</sub> plume

Heterogeneous scenario of site-S does not seem to affect the results of spatio-temporal extent of pressure buildup and saturation as shown in Figs. 8 and 9. Cyclic injection scheme introduces fluctuations in the areal extent of both pressure buildup and saturation, while other three injection schemes show a smooth variation in areal extent of pressure buildup

and CO<sub>2</sub> saturation. The extent of pressure buildup for  $P > 0.01$  MPa was negligible, therefore, the three legends for  $P = 0.1, 0.5, 1.0$  MPa are not visible in Fig. 8.

#### 3.2.2 Variability in pressure buildup and saturation

The results shown in Figs. 10 and 11 follow exactly the same behavior as observed under homogeneous case, with small differences introduced as a result of heterogeneity. For example in Fig. 10, the results for stepwise increasing and stepwise decreasing injection schemes also show some fluctuations with time that were not present in the case of homogeneous geology. These fluctuations in the case of stepwise increasing and stepwise decreasing injection schemes are possibly introduced due to lateral shale layers with discontinuities in the form of perforations/baffles that stops the CO<sub>2</sub>, but an increase or decrease in injection rate changes the local pressure gradient that allows the CO<sub>2</sub> to move towards the baffles and then rise above due to buoyancy. However, these moderate fluctuations in pore pressure introduced by stepwise increasing and stepwise decreasing injection schemes are not observed in the saturation plume as shown by Fig. 11.



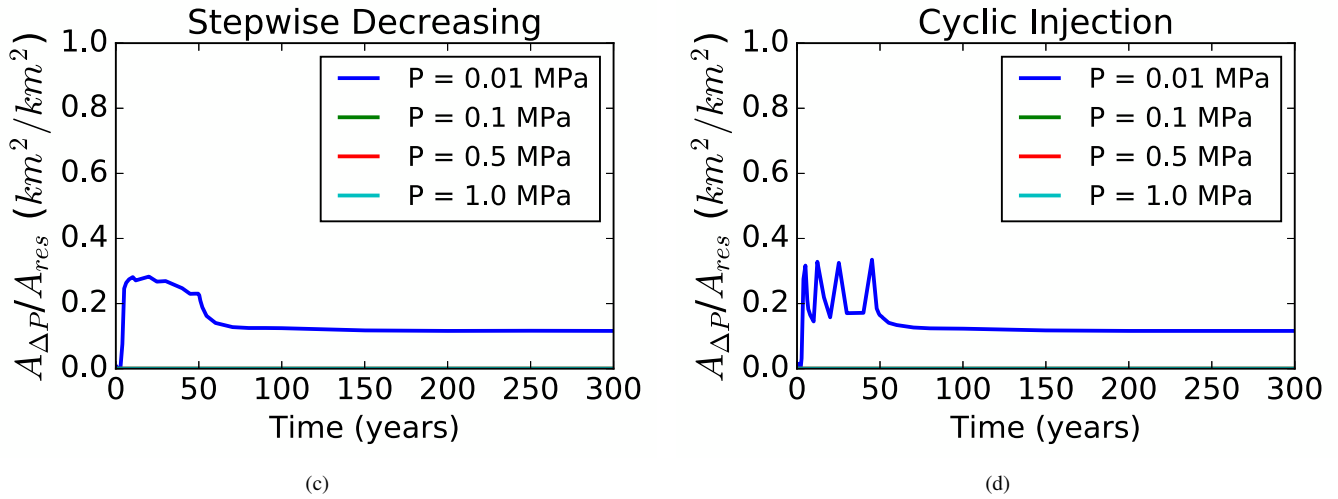


Fig. 8.  $A_{\Delta P}(t)/A_{res}$  with constant, stepwise increasing, stepwise decreasing, and cyclic injection rates.

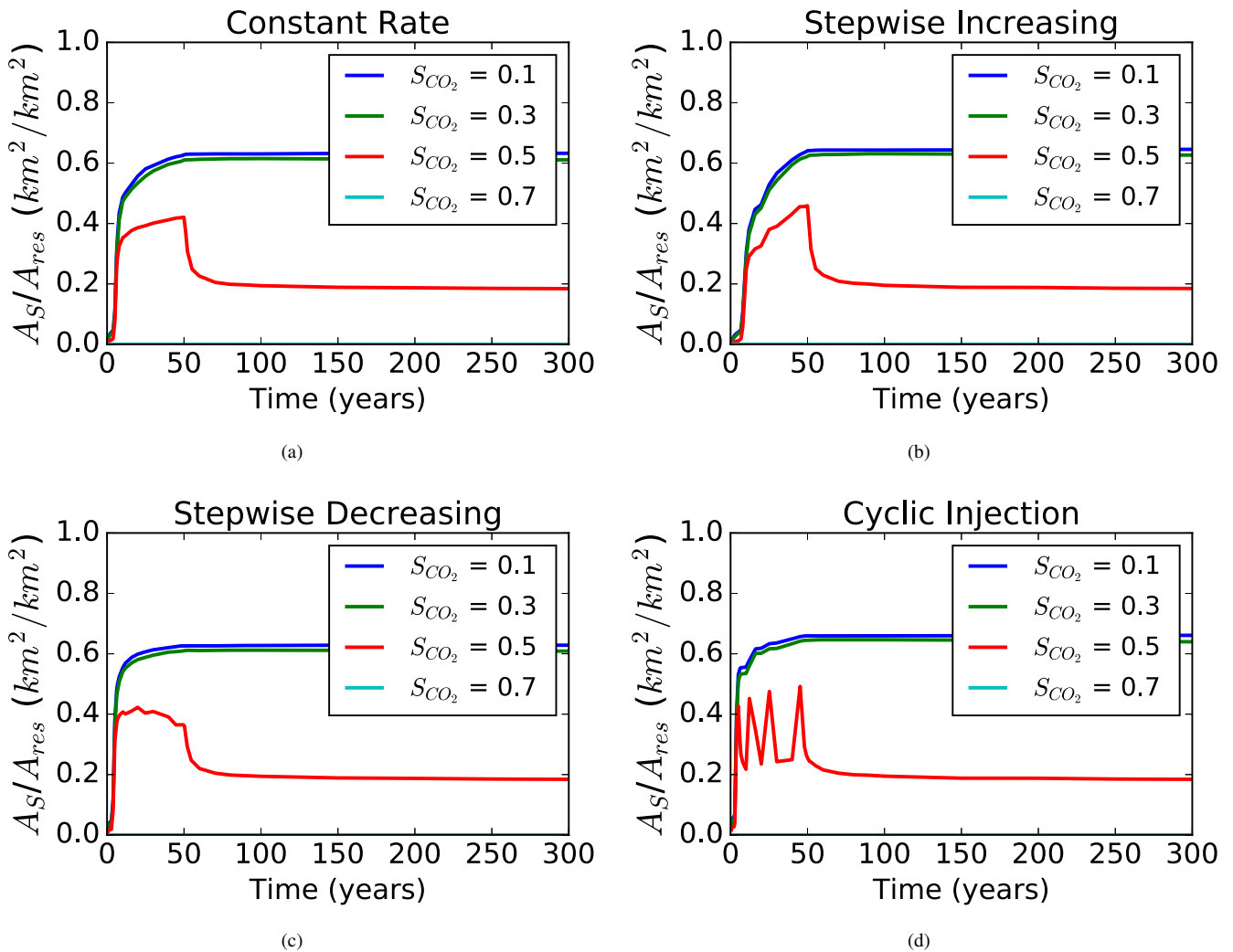


Fig. 9.  $A_S(t)/A_{res}$  with constant, stepwise increasing, stepwise decreasing, and cyclic injection rates.

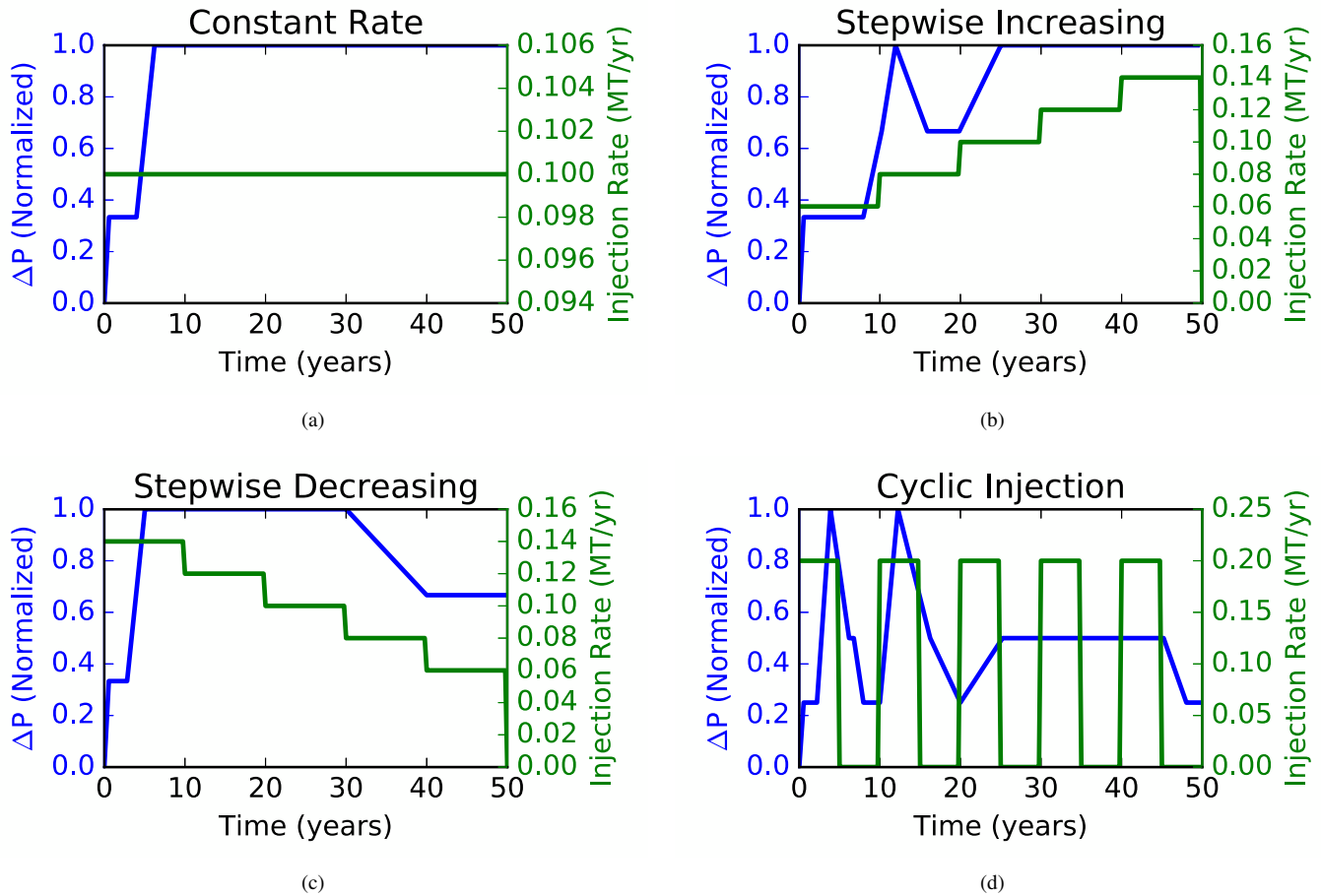


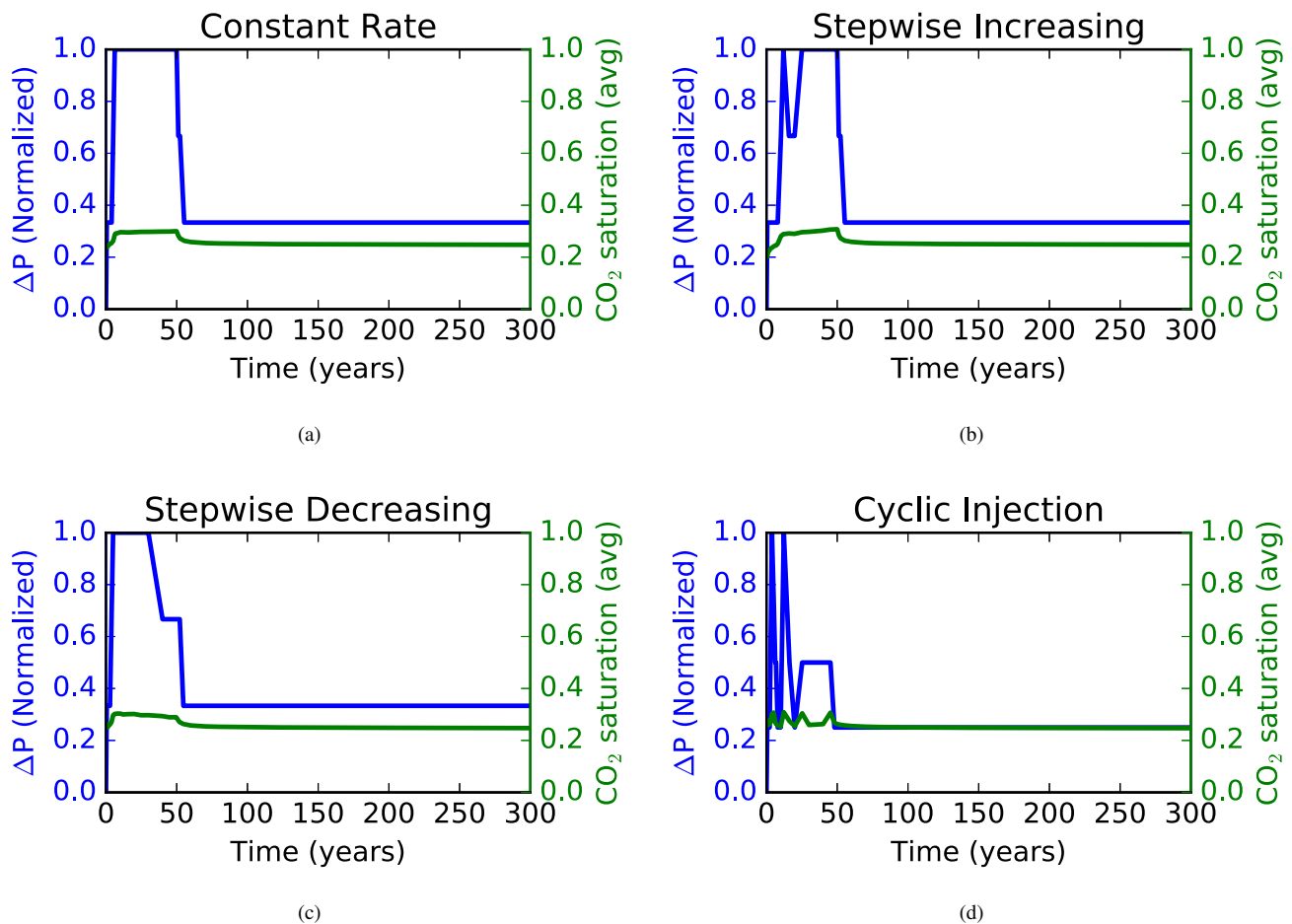
Fig. 10. Average pore pressure and injection rates with constant, stepwise increasing, stepwise decreasing, and cyclic injection rates.

### 3.3 Effect of boundary conditions

The pressure buildup with the open-flow boundary condition (allowing both the  $\text{CO}_2$  and brine to flow out freely through initial reservoir pressure) is not very large ( $< 1$  MPa), but the magnitude of pressure buildup increases with the increase in flow region's boundaries. This observation has been discussed by other studies (Doughty, 2009; Zhang et al., 2016), which reported that location of the boundary (flow region of the reservoir) relative to plume extent can have a very significant contribution on pressure buildup on  $\text{CO}_2$  injection. However, boundaries do not play an important role if the flow region of the model is large for the pressure perturbation to reach its boundaries (e.g., Birkholzer and Zhou, 2009; Doughty, 2009; Zhou et al., 2009; Smith et al., 2011; Zhou and Birkholzer, 2011; Schäfer et al., 2012; Zhang et al., 2016). Closed boundary conditions are expected to result in general (average) pressure increase in the storage system, while in comparison open-flow boundaries are less susceptible to pressure increase except if there are multiple injectors that can cause pressure interference (e.g., Birkholzer and Zhou, 2009; Zhou and Birkholzer, 2011) depending on the spacing of the wells and the reservoir size.

### 4. Summary and conclusions

This study investigated the spatio-temporal extent of pressure buildup and  $\text{CO}_2$  saturation plume as a function of four different injection schemes (constant rate, stepwise increasing rate, stepwise decreasing rate, and cyclic rate) to understand how the variation in injection rate, by constraining the cumulative amount stored, affects the reservoir risk. Spatio-temporal extent of pressure buildup and  $\text{CO}_2$  saturation plume were obtained for four injection schemes, considering both homogeneous and heterogeneous geology of the site. Results showed that cyclic injection tends to keep the pore pressure lower than the other three injection schemes, while the highest pressure increase over the entire injection period (50 years) is observed with stepwise decreasing rate. The compressibility of  $\text{CO}_2$  plays a role in attenuating the impact of fluctuating cyclic injection signals on pressure after 30 years of injection, where this time decreases by 5 years in case of heterogeneous scenario. Although cyclic fluctuations in the pressure (by cyclic injection rate) are also mimicked by the  $\text{CO}_2$  saturation, they are not as pronounced as the fluctuations in pressure. Layered heterogeneity of the model introduces small differences compared to the homogeneous case in a way that stepwise increasing and stepwise decreasing injection schemes also show some fluctuations in pore pressure with time, but these fluctuations are not observed in the saturation plume.



**Fig. 11.** Average pore pressure and average saturation with constant, stepwise increasing, stepwise decreasing, and cyclic injection rates.

However, layered heterogeneity of site-S did not affect the areal extent of the pressure buildup or the saturation.

These results have important implications for storage reservoirs that may be prone to high pressure buildup during injection because of their geology, for instance fractured shale reservoirs (Myshakin et al., 2018; Singh and Cai, 2018), such that it would be preferable to store CO<sub>2</sub> using a cyclic injection scheme that will keep the pore pressure lower than the other three injection schemes. These results also carry important implications for enhanced oil recovery (EOR) using CO<sub>2</sub> where the primary goal is to drive the oil out by increasing pore pressure; for EOR by CO<sub>2</sub>, stepwise decreasing rate would be most preferable as it leads to highest increase in pore pressure.

It has been shown in the context of oil recovery (Song and Yang, 2013; Yu et al., 2016) by huff-n-puff, which mimics a cyclic injection, shut-in time does not have any effect on the oil recovery except that the short shut-in time (or soaking time) recovers the oil faster. In the context of pressure buildup, it is apparent from Figs. 6 and 10 that a shorter shut-in time (or soaking period) for the cyclic injection may lead to a lower drop in the pressure built up during injection and a larger shut-in time may lead to a larger drop in the pressure built up during injection.

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